## BIRLA INSTITUTE OF TECHNOLOGY AND SCIENCE, PILANI First Semester 2023-2024 (9/12/2023)

Co	omprehensive Examination (PART A-Closed book-45 ma	rks, suggested time 130 min)				
Course No. : CH	E F422	Total time: 180 min				
Course Title: PR	Т	Total Marks: 60				
Instructions:	Number each main question correctly					
	Start each new main answer on a fresh page					
Part B (open book) answer booklet may only be taken once part A answer booklet is s						
	Time distribution for Part A and B is up to the student					

**Q1**. The following fig. A & B are important components of two refinery processes. For **each case (separately)** answer:



Q2. Carefully observe the figure below. It is a simplified flowsheet of a refinery process. Answer the given questions:



**Q3**. The following graph of **aromatics hydrogenation%** (**y-axis**) Vs T (x-axis) shows reaction effects for a processing unit. Give (a) Unit name and main purpose. (b) Operating T, P (c) catalyst (d) Explain trend of given graph. **[5]** 



Q4 the following conventional box-type furnace (cabin heater) is being used to heat feed for an ADU. Now the daily feed volume rate increases by 50%. If the main construction of the furnace (volume) cannot be changed, what other modifications can be done to accommodate the increased daily capacity requirement? Assume that the temperature requirement of the furnace output is required to be the same as before. [4]



Q5) Give the complete name of Test 1 and Test 2 from the schematic of the test set-up for crude fractions, and briefly describe purpose of each test and the fuel for which it is usually used. [2+2=4]

**Q5**. **Give** *only* **the significance** of these properties for the fuel that they define: (a) Pour point (b) Viscosity Index (c) Octane number (RON & MON) (d) Wobbe Number. **[4]** 

Q6. What is the difference between the two terms on the basis provided in brackets? Go directly to the point (4×2=8)

- 1) Shale fracking, oil drilling (process)
- 2) Organic theory, peak oil theory (evidence for these theories)
- 3) Resin, asphaltene/ Bitumen (end use in our country)
- 4) Gasoline, Hydrogen (explosive limit range, i.e. difference in upper and lower explosive limits, volume% in air)

(PART B-Open book-15 marks, suggested time 50 min)

Instructions:	Write all the steps of the solution procedure and quote all data sources.
	Show at least one sample calculation for each column data.

- (i) TBP data for a Brent blend (°API= 41.1) is reported in Table-1. Find K for the whole crude, and comment on the value. [5]
- (ii) For the four separations made in ADU, the TBP cut temperatures (T<sub>cut</sub>) and separation capacities (F) are reported in Table-2. In an attempt at heat integration within the petroleum refinery complex, lights from another column were injected into the bottom cut (B) to add heat (in place of reboiler). The resultant local mixing caused the bottom cut to become slightly lighter, with a t<sub>50%</sub> value of 735 °F (the injected lights had very less flowrate and did not affect anything else in the column). For each separation, the Δt<sub>50%</sub> and ASTM Gaps/ Overlap (use -/+ to indicate which) as indicated in Table-2. [10]

Та	ble-	1

Vol. %	0	5	10	20	30	40	50	60	70	80
TBP, ° F	-130	148	213	327	430	534	639	747	867	1013

Table-2

Sl. No	Separation	T <sub>cut</sub> (°F)	F for section	Find each	Find each
				$\Delta t_{50\%}$	Gap/overlap
1	D <sub>3</sub> -(D <sub>4</sub> +V <sub>4</sub> )	255	40	а	А
2	D <sub>2</sub> -D <sub>3</sub>	365	30	b	В
3	D1-D2	545	10	с	С
4	B-D <sub>1</sub>	650	10	d	D